Prediction of the fluid phase behavior of the quaternary system ethylene oxide + air by molecular simulation

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According to the vision of the Industrial Fluid Property Simulation Collective (IFPSC), "molecular simulation will become a breakthrough technology that is widely accepted in the chemical industry and applied (...) to meet the industry's evolving fluid property data needs" [1]. This is of particular interest for hazardous fluids which are economically vital, but often little explored experimentally. In 2007, IFPSC has therefore challenged the development of new molecular models for such a substance, i.e. ethylene oxide (EO) [2]. The response of the community has shown that state-of-the-art molecular models are indeed capable of quantitatively covering a wide range of thermodynamic properties in a predictive manner. The present contribution is built upon the EO model developed in our group [3], which was the first entry of the challenge. It agrees almost throughout with the available reference data, taking the combined error bars into account.

As stated in [2], there is generic interest in the fluid phase behavior as well as the compressed liquid density of the mixture EO + air and its subsystems.

In this work, the molecular model for EO [3] is combined with a ternary model for air [4]. Two of the three unlike interactions affecting EO (with nitrogen and with argon) were calibrated to experimental Henry's law data, altering the dispersion energy by less

than 4% from the Lorentz-Berthelot rule. On the basis of this model, the vapor-liquid equilibrium was predicted for the quaternary system and all its binary and ternary subsystems for a broad range of temperatures and pressures. Furthermore, compressed liquid densities are predicted as well. In order to facilitate the use of these data for subsequent work, cubic equations of state were parameterized to the whole set of simulation data. In total, this case study aims to present a straightforward route to include molecular simulation into industrial applications.

[1] http://www.fluidproperties.org/

[2] F. H. Case, J. Brennan, A. Chaka, K. D. Dobbs, D. G. Friend, P. A. Gordon, J. D. Moore, R. D. Mountain, J. D. Olson, R. B. Ross, M. Schiller, V. K. Shen, and E. A. Stahlberg, Fluid Phase Equilib. 274: 2-9 (2008).

[3] B. Eckl, J. Vrabec, and H. Hasse, Fluid Phase Equilib. 274: 16-26 (2008).

[4] J. Vrabec, G. K. Kedia, and H. Hasse, Cryogenics 45: 253-258 (2005).